2330 PHYSICAL AND AGGREGATE PROPERTIES OF WATER AND WASTEWATER; Calcium Carbonate Saturation

Select the smaller value of P or (T-P). Then, carbonate alkalinity equals twice the smaller value. When the smaller value is P, the balance (T-2P) is bicarbonate. When the smaller value is (T-P), the balance (2P-T) is hydroxide. All results are expressed as  $CaCO_3$ . The mathematical conversion of the results is shown in Table 2320:2. (A modification of Table 2320:2 that is more accurate when  $P \simeq \frac{1}{2}T$  has been proposed.<sup>4</sup>)

Alkalinity relationships also may be computed nomographically (see Carbon Dioxide, Section 4500-CO<sub>2</sub>). Accurately measure pH, calculate OH<sup>-</sup> concentration as milligrams CaCO<sub>3</sub> per liter, and calculate concentrations of CO<sub>3</sub><sup>2-</sup> and HCO<sub>3</sub> as milligrams CaCO<sub>3</sub> per liter from the OH<sup>-</sup> concentration, and the phenol-phthalein and total alkalinities by the following equations:

$$CO_3^{2-} = 2P - 2[OH^-]$$

$$HCO_3^- = T - 2P + OH^-$$

Similarly, if difficulty is experienced with the phenolphthalein endpoint, or if a check on the phenolphthalein titration is desired, calculate phenolphthalein alkalinity as CaCO<sub>3</sub> from the results of the nomographic determinations of carbonate and hydroxide ion concentrations:

$$P = 1/2 \left[ CO_3^{2-} \right] + \left[ OH^- \right]$$

# 6. Precision and Bias

No general statement can be made about precision because of the great variation in sample characteristics. The precision of the titration is likely to be much greater than the uncertainties involved in sampling and sample handling before the analysis.

In the range of 10 to 500 mg/L, when the alkalinity is due entirely to carbonates or bicarbonates, a standard deviation of 1 mg/L CaCO<sub>3</sub> can be achieved. Forty analysts in 17 laboratories analyzed

synthetic samples containing increments of bicarbonate equivalent to 120 mg/L CaCO<sub>3</sub>. The titration procedure of 2320 B.4*b* was used, with an endpoint pH of 4.5. The standard deviation was 5 mg/L and the average bias (lower than the true value) was 9 mg/L.<sup>5</sup>

Sodium carbonate solutions equivalent to 80 and 65 mg/L CaCO<sub>3</sub> were analyzed by 12 laboratories according to the procedure of 2320 B.4c.<sup>6</sup> The standard deviations were 8 and 5 mg/L, respectively, with negligible bias.<sup>6</sup> Four laboratories analyzed 6 samples having total alkalinities of about 1000 mg/L CaCO<sub>3</sub> and containing various ratios of carbonate:bicarbonate by the procedures of both 2320 B.4a and c. The pooled standard deviation was 40 mg/L, with negligible difference between the procedures.

#### References

- 1. Larson TE, Henley LM. Determination of low alkalinity or acidity in water. Anal Chem. 1955;27(5):851–852.
- Thomas JFJ, Lynch JJ. Determination of carbonate alkalinity in natural waters. J Amer Water Works Assoc. 1960;52(2):259–268.
- Cooper SS. The mixed indicator bromocresol green-methyl red for carbonates in water. Ind Eng Chem Anal Ed. 1941;13(7):466– 470.
- Jenkins SR, Moore RC. A proposed modification to the classical method of calculating alkalinity in natural waters. J Amer Water Works Assoc. 1977;69(1):56–60.
- Winter JA, Midgett MR. FWPCA method study 1: Mineral and physical analyses. Washington DC: Federal Water Pollution Control Administration; 1969.
- Smith R. Research Rep. No. 379. South Africa: Council for Scientific and Industrial Research; 1980.

## Bibliography

American Society for Testing and Materials. Standard methods for acidity or alkalinity of water; Pub. D1067-70 (reapproved 1977). Philadelphia, (PA): ASTM International; 1982.

Skougstad MW, Fishman MJ, Friedman LC, Erdman DE, Duncan SS. Methods for determination of inorganic substances in water and fluvial sediments. In: Techniques of water-resources investigation of the United States Geological Survey. Washington DC: U.S. Geological Survey; 1979, Book 5, Chapter A1.

# 2330

# CALCIUM CARBONATE SATURATION

Approved by Standard Methods Committee, 2016. Editorial revisions, 2021. Joint Task Group: John D. Kenny (chair), Paul J. Kemp, Devon A. Morgan, Stephen J. Randtke, William R. Ray, Ravindra M. Srivastava, Lawrence K. Wang.

(2330) A. Introduction

## 1. General Discussion

Calcium carbonate (CaCO<sub>3</sub>) saturation indices are commonly used to evaluate a water's scale-forming and scale-dissolving tendencies to help prevent CaCO<sub>3</sub> scaling in piping and equipment (e.g., industrial heat exchangers or domestic water heaters). The

indices can be applicable in reducing corrosion in iron, steel, and cement piping, but not in controlling lead and copper release.

Water oversaturated with CaCO<sub>3</sub> tends to precipitate CaCO<sub>3</sub>. Water undersaturated with CaCO<sub>3</sub> tends to dissolve it. Saturated water (i.e., water in equilibrium with CaCO<sub>3</sub>) tends neither to precipitate nor dissolve CaCO<sub>3</sub>. Saturation is the dividing line

between where precipitation tends to occur (likely) or not occur (not likely). Dissolved total alkalinity (Section 2320), total calcium (Section 3500-Ca), pH (Section 4500-H<sup>+</sup>), and temperature (Section 2550) must be measured to calculate the CaCO<sub>3</sub> saturation indices described here. Ionic strength also must be calculated or estimated from total dissolved solids (TDS) (Section 2540 C) or conductivity (Section 2510) measurements.

Measure pH at the system's water temperature using a temperature-compensated pH meter. If pH is measured at a different temperature in the laboratory, for example, correct the measured pH. <sup>1-7</sup> When measuring pH, minimize CO<sub>2</sub> exchange between sample and atmosphere. Ideally, seal the sample from the atmosphere during measurements. <sup>8</sup> At a minimum, avoid vigorously stirring unsealed samples.

There are two general categories of CaCO<sub>3</sub> saturation indices:

- indices that determine whether a water has a *tendency* to precipitate or to dissolve CaCO<sub>3</sub>, and
- indices that estimate the quantity of CaCO<sub>3</sub> that can be precipitated or dissolved.

## 2. Limitations

It is widely assumed that CaCO<sub>3</sub> precipitates from oversaturated waters and cannot be deposited by undersaturated waters, but there are exceptions. For example, phosphates (particularly polyphosphates), certain naturally occurring organics, sulfate, magnesium, and some trace metals (e.g., zinc) can act as sequestering agents or crystal poisons, inhibiting oversaturated waters from depositing CaCO<sub>3</sub>.<sup>9-12</sup> Conversely, CaCO<sub>3</sub> deposits have been found in pipes conveying undersaturated water due to high pH (relative to bulk water pH) next to certain areas (cathodes) of corroding metal surfaces. Even if the bulk water is undersaturated, a locally oversaturated condition can cause a small, but significant, amount of CaCO<sub>3</sub> to be deposited.

The calculations referred to here—even the most sophisticated computerized calculations—do not adequately describe these exceptions, so do not consider saturation indices as absolutes. Rather, view them as guides to the behavior of CaCO<sub>3</sub> in aqueous systems and supplement them, where possible, with experimentally derived information.

Waters with positive indices are sometimes assumed to be protective, while waters with negative indices are sometimes assumed to be corrosive. In actuality, this relationship is observed with some materials, 13,14 but not with others. 15,16 The indices can relate to corrosion rates through the clogging of reactive areas by CaCO<sub>3</sub> precipitation, which can provide a matrix to retain corrosion products, further sealing surfaces. Calcium carbonate scales can reduce corrosion of unlined iron pipe; however, water characteristics not directly involved in calculating the indices [e.g., dissolved oxygen (DO), buffering intensity, chloride, sulfate, and water velocity] can influence corrosion rates appreciably. 12,14,17-22 Calcium carbonate scales can also reduce the release of free lime in cement-mortar-lined and asbestos-cement pipes. Significant CaCO3 films rarely deposit on lead, galvanized, and copper cold-water pipes. 12,22 Calcium carbonate saturation indices are not predictive of corrosion for lead, copper, or leaded brass pipes. 23-25 While the U.S. Environmental Protection Agency required community water-supply systems to determine CaCO<sub>3</sub> saturation indices from 1980 to 1994, the requirement was appealed in 1994 due to misuse as corrosion indices.<sup>25</sup>

- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. I. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(11):592–599.
- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. II. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(12):634–640.
- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. III. A practical approach for plant operators. J Amer Water Works Assoc. 1978;70(1):12–18.
- Loewenthal RE, Marais GVR. Carbonate chemistry of aquatic systems: theory and applications. Ann Arbor (MI): Ann Arbor Science Publishers, 1976.
- Merrill DT. Chemical conditioning for water softening and corrosion control. In: Sanks RL, ed. Water treatment plant design. Ann Arbor (MI): Ann Arbor Science Publishers, 1976.
- American Water Works Association Research Foundation. Lead Control Strategies; Appendix G. Denver (CO): American Water Works Association Research Foundation and American Water Works Association; 1990.
- Trussell RR, Kenny JD, Hokanson DR. Correcting for temperature when calculating calcium carbonate saturation. J Amer Water Works Assoc. 2016;108(8):E454–457.
- Schock MR, Mueller W, Buelow RW. Laboratory technique for measurement of pH for corrosion control studies and water not in equilibrium with the atmosphere. J Amer Water Works Assoc. 1980;72(5):304–306.
- Pytkowicz RM. Rates of inorganic carbon nucleation. J Geol. 1965;73:196–199.
- Ferguson JF, McCarty PL. Precipitation of phosphate from fresh waters and waste waters; Technical Report No. 120. Stanford University; 1969.
- Merrill DT, Jorden RM. Lime-induced reactions in municipal wastewaters. J Water Pollut Control Fed. 1975;47(12):2783–2808.
- Schock MR, Lytle DA. Internal corrosion and deposition control. In: Edzwald JK, ed. Water quality and treatment, 6th ed. New York (NY): McGraw Hill; 2011.
- De Martini FE. Corrosion and the Langelier calcium carbonate saturation index. J Amer Water Works Assoc. 1938;30(1):85–111.
- Larson TE. Corrosion by domestic waters; Bulletin 59. Illinois State Water Survey; 1975.
- James M. Montgomery, Consulting Engineers, Inc. Water treatment principles and design. New York (NY): John Wiley & Sons; 1985.
- Stumm W. Investigations of the corrosive behavior of waters. J Sanit Engineer Div. 1960;86(6):27–46.
- Pisigan RA Jr, Singley JE. Evaluation of water corrosivity using the Langelier index and relative corrosion rate models. Materials Perform. 1985;24(4):26–36.
- Lane RW. Control of corrosion in distribution and building water systems. In: Proceedings of the AWWA Water Quality Technology Conference 1982 Dec. 5–8; Nashville (TN). Denver (CO): American Water Works Association; 1982.
- Sontheimer H, Kolle W, Snoeyink VL. The siderite model of the formation of corrosion-resistant scales. J Amer Water Works Assoc. 1982;73(11):572–579.
- Schock MR, Neff CH. Chemical aspects of internal corrosion; theory, prediction, and monitoring. In: Proceedings of the AWWA Water Quality Technology Conference 1982 Dec. 5–8; Nashville (TN). Denver (CO): American Water Works Association; 1982.
- 21. American Water Works Association. Corrosion control for plant operators; ISBW-O-89867-350-X. Denver (CO): AWWA; 1986.

- American Water Works Association Research Foundation. 1996.
   Internal corrosion of water distribution systems, 2nd ed.; ISBWO-89867-759-9. Denver (CO): AWWA; 1996.
- Edwards M, Schock MR, Meyer TE. Alkalinity, pH, and copper corrosion by-product release. J Amer Water Works Assoc. 1996;88(3):81–94.
- DeSantis MK, Schock MR. Ground truthing the 'conventional wisdom' of lead corrosion control using mineralogical analysis. In:
- Proceedings of the AWWA Water Quality Technology Conference; 2014 Nov 16–19; New Orleans (LA). Denver (CO): Amer Water Works Association; 2014.
- Schock MR, Lytle DA. Internal corrosion and deposition control. In: Edzwald JK, ed. Water quality and treatment: a handbook of community water supplies, 6th ed. New York (NY): McGraw-Hill, Inc.; 2011.

# (2330) B. Indices Indicating a Water's Tendency to Precipitate or Dissolve CaCO<sub>3</sub>

# 1. General Discussion

Indices that indicate CaCO<sub>3</sub> precipitation or dissolution tendencies define whether a water is oversaturated, saturated, or undersaturated with CaCO<sub>3</sub>. The most widely used indices are the Saturation Index (SI), Relative Saturation (RS) [also known as the *Driving Force Index* (DFI) and the *Saturation Ratio* (SR)], and the Ryznar Index (RI). The SI is by far the most commonly used and is described here.

The RS and SI are related (2330 D.1, Equation 7). The RI<sup>1</sup> has been used for many years, sometimes with good results. Because it is semi-empirical, however, it may be less reliable than the SI.

# 2. Saturation Index by Calculation

SI is determined from Equation 1:

$$SI = pH - pH_{s} \tag{1}$$

where:

pH = measured pH, and

 $pH_s = pH$  of the water if it were in equilibrium with CaCO<sub>3</sub> at the existing calcium ion [Ca<sup>2+</sup>] and bicarbonate ion [HCO<sub>3</sub>] concentrations.

Table 2330:1. Estimating Equilibrium Constants and Activity Coefficients

Equation	Temperature Range (K)	References
When complete mineral analysis is available:		
i	_	1
$I = 1/2 \sum_{i=1}^{l} [X_i] Z_i^2$		
<i>i</i> =1		
When a complete mineral analysis is not available: $I = TDS/40,000$	_	2
When only conductivity is available: $I = 1.6 \times 10^{-5} C$	· –	3
	_	1
$pf_m = A \left[ \frac{\sqrt{I}}{1 + \sqrt{I}} - 0.3I \right] $ (valid to $I < 0.5$ )		
$[1+\sqrt{I}]$		
$A = 1.82 \times 10^6  (ET)^{-1.5}$	<u></u>	1
$E = 308.67e^{-0.0045976(T)}$	273–373	4
$pK_1 = 356.3094 + 0.06091964 T - 21834.37/T - 126.8339 \log_{10}T + 1684915/T^2$	273–373	5
$pK_2 = 107.8871 + 0.03252849 T - 5 151.79/T - 38.92561 \log_{10}T + 563 713.9/T^2$	273–373	5 .
$pK_{w} = 4470.99/T + 0.017060 T - 6.0875$	273–333	6
$pK_{sc} = 171.9065 + 0.077993 T - 2839.319/T - 71.595 \log_{10}T$	273–363	5
$pK_{sa} = 171.9773 + 0.077993 T - 2.903.293/T - 71.595 \log_{10}T$	273–363	5
$pK_{sv} = 172.1295 + 0.077993 T - 3.074.688/T - 71.595 \log_{10}T$	273–363	5

I= ionic strength;  $[X_i]=$  concentration of component i (moles/L);  $Z_i=$  charge of species i; TDS= total dissolved solids (mg/L); C= conductivity ( $\mu$ mhos/cm);  $pY=-\log_{10}$  of the value of any factor Y;  $f_m=$  activity coefficient for monovalent species; E= dielectric constant; T= temperature, K (°C + 273.15);  $K_1=$  first dissociation constant for carbonic acid, including  $CO_{2(aq)}$ ;  $K_2=$  second dissociation constant for carbonic acid;  $K_w=$  dissociation constant for water;  $K_{sc}=$  solubility product constant for calcite;  $K_{sa}=$  solubility product constant for aragonite;  $K_{sv}=$  solubility product constant for vaterite.

- 1. Stumm W, Morgan JJ. Aquatic Chemistry, 3rd ed. New York (NY): John Wiley & Sons; 1996.
- 2. Langelier WF. The analytical control of anticorrosion water treatment. J Amer Water Works Assoc. 1936;28(10):1500–1521.
- 3. Russell LL. Chemical aspects of groundwater recharge with wastewaters [Ph.D. thesis] University of California, Berkeley; 1976.
- Russett E.L. Chemical aspects of groundwater rectarge with wastewaters in the stress of charge of caution and precipitation, and precipitative softening. In: Edzwald JK, ed. Water quality & treatment: a handbook on drinking water, 6th ed. McGraw Hill, New York, N.Y. 2011, p. 13.26.
- 5. Plummer LN, Busenberg E. The solubilities of calcite, aragonite, and vaterite in CO2-H2O solutions between 0 and 90°C, and an evaluation of the aqueous model for the system CaCO3-CO2-H2O. Geochim Cosmochim Acta. 1982;46(6):1011–1040.
- 6. Harned HS, Owen BB. The physical chemistry of electrolytic solutions, 3rd ed. New York, (NY): Reinhold Publishing Corp.; 1958.

If SI is positive, the water is oversaturated with CaCO<sub>3</sub>; if negative, the water is undersaturated. If SI is zero, the water is in equilibrium with CaCO<sub>3</sub>.

a. Analytical solution for  $pH_s$ : Determine  $pH_s$  as follows:<sup>2</sup>

$$pH_s = pK_2 - pK_s + p\left[\text{Ca}^{2+}\right] + p\left[\text{HCO}_3^{-}\right] + 5 \, pf_m$$
 (2)

where:

p= when preceding a variable, designates  $-\log_{10}$  of that variable,  $K_2=$  second dissociation constant for carbonic acid at water temperature.

 $K_s$  = solubility product constant for CaCO<sub>3</sub> at water temperature,

 $[Ca^2+]$  = calcium ion concentration (moles/L),

[HCO3-] = bicarbonate ion concentration (moles/L), and

 $f_m$  = activity coefficient for monovalent species at the specified temperature.

Using the equations in Table 2330:1, calculate the values of  $pK_2$ ,  $pK_s$ , and  $pf_m$  required to solve Equation 2. To save computation time, values for  $pK_2$  and  $pK_s$  have been precalculated for selected temperatures (Table 2330:2). Table 2330:2 gives several values for  $pK_s$  because different isomorphs of CaCO<sub>3</sub> (e.g., calcite, aragonite, and vaterite) can form in aqueous systems, and each has somewhat different solubility properties. To accommodate for such differences when computing  $pH_s$ , use the  $pK_s$  for the compound most likely to form. For example, calcite is the form of CaCO<sub>3</sub> most commonly found in fresh water.

Estimate the calcium ion concentration from total calcium measurements as follows:

$$\left[Ca^{2+}\right] = Ca_t - Ca_{ip} \tag{3}$$

where:

 $Ca_t = \text{total calcium (moles/L)}$  and

 $Ca_{ip}$  = calcium associated with ion pairs (e.g., CaHCO<sub>3</sub><sup>+</sup>, CaSO<sub>4</sub><sup>0</sup>, and CaOH<sup>+</sup>).

Calcium associated with ion pairs is not available to form CaCO<sub>2</sub>.

Estimate [HCO<sub>3</sub>], the bicarbonate ion concentration, as follows:<sup>3</sup>

$$\left[\text{HCO}_{3}^{-}\right] = \frac{Alk_{t} - Alk_{0} + 10^{\left(pf_{m} - pH\right)} - 10^{\left(pH + pf_{m} - pK_{w}\right)}}{1 + 2 \times 10^{\left(pH + 3pf_{m} - pK_{2}\right)}}$$
(4)

where:

 $Alk_t$  = total alkalinity, as determined by acid titration to the carbonic acid endpoint, equivalents/L;

Alk<sub>o</sub> = alkalinity contributed or consumed by NH<sub>3</sub>, H<sub>3</sub>SiO<sub>4</sub><sup>-</sup>, H<sub>2</sub>SiO<sub>4</sub><sup>2</sup>-, HPO<sub>4</sub><sup>2</sup>-, PO<sub>4</sub><sup>3</sup>-, H<sub>3</sub>PO<sub>4</sub>, B(OH)<sub>4</sub><sup>-</sup>, CH<sub>3</sub>COO<sup>-</sup> (acetate), HS<sup>-</sup>, S<sup>2</sup>-, ion pairs (e.g., CaHCO<sub>3</sub><sup>+</sup> and MgOH<sup>+</sup>), and other species that neutralize strong acid when titrating to the carbonic acid endpoint, which can include organic acids (e.g., fulvic and humic acids) with equivalents/L contributions that are usually small compared to those of (HCO<sub>3</sub><sup>-</sup>, CO<sub>3</sub><sup>2</sup>-, OH<sup>-</sup>, and H<sup>+</sup>); and

 $K_{w}$  = dissociation constant for water, at water temperature.

Calculations can be simplified. In Equation 4 for example, terms containing exponents [e.g.,  $10^{(pH+ppn-pkw)}$ ] usually can be neglected for waters whose pH is 6.0 to 8.5 and alkalinity is more than about 50 mg/L as CaCO<sub>3</sub>. The terms  $Ca_{ip}$  in Equation 3 and  $Alk_o$  in Equation 4 are difficult to calculate without computers, so they usually are neglected in hand calculations. The simplified version of Equation 2 under such conditions is:

$$pH_s = pK_2 - pK_s + p[Ca_t] + p[Alk_t] + 5pf_m$$
(5)

1) Sample calculation—The calculation is best illustrated by working through an example. Assume that calcite controls CaCO<sub>3</sub> solubility, and determine the SI for a water with the following composition:

Constituent	Calculate Molar Concentration (mg/L ÷ mg/mole = moles/L)					
Calcium	152	40 078	$3.79 \times 10^{3}$			
Magnesium	39	24 305	$1.60 \times 10^{3}$			
Sodium	50	22.990	$2.17 \times 10^{3}$			
Potassium	5	39 098	$1.28 \times 10^{4}$			
Chloride	53	35 450°	$1.50 \times 10^{3}$			
Alkalinity (as CaCO <sub>3</sub> )	130	50 000b	$2.60 \times 10^{3c}$			
Sulfate	430	96 060ª	$4.48 \times 10^{-3}$			
Silica (as SiO <sub>2</sub> )	15	60 083ª	$2.50 \times 10^{-3}$			

<sup>a</sup> Based on conventional atomic weights. See Haynes WM, ed. CRC handbook of chemistry and physics, 96th ed. Boca Raton (FL): CRC Press; 2015.

c Equivalents/L.

Note: Water temperature = 20 °C (293.15K); pH = 9.00.

Before evaluating  $pf_m$  in Equation 2, determine the ionic strength (*I*) and another constant (*A*). Using the first equation in Table 2330:1, estimate the ionic strength assuming all the alkalinity is due to bicarbonate ion (an assumption that introduces only a small error at pH 9.00). Use the alkalinity concentration (2.60  $\times$  10<sup>-3</sup>) and the bicarbonate charge (-1) to calculate alkalinity's contribution to ionic strength. Likewise, assume silica is mostly  $H_4SiO_4$  at pH 9.00, as the other species typically can be neglected when pH is  $\leq$  9. Because  $H_4SiO_4$  has zero charge, it does not contribute to ionic strength.

$$\begin{split} I &= \frac{1}{2} \sum_{i=1}^{i} [X_i] Z_i^2 = 0.5 \times \left[ \left( 3.79 \times 10^{-3} \right) \times 2^2 + \left( 1.60 \times 10^{-3} \right) \times 2^2 \right. \\ &+ \left( 2.17 \times 10^{-3} \right) \times 1^2 + \left( 1.28 \times 10^{-4} \right) \times 1^2 + \left( 1.50 \times 10^{-3} \right) \times 1^2 \\ &+ \left( 2.60 \times 10^{-3} \right) \times 1^2 + \left( 4.48 \times 10^{-3} \right) \times 2^2 \right] = 2.29 \times 10^{-2} \text{ moles / L} \end{split}$$

In the absence of a complete water analysis, estimate ionic strength from TDS measurements or, as a last resort, from conductivity (see alternative equations in Table 2330:1).

<sup>&</sup>lt;sup>b</sup> Although a more accurate value of the equivalent weight of CaCO<sub>3</sub> can be calculated from standard atomic weights, a value of 50 000 should be used because that is the value used to convert the results of an alkalinity titration into an alkalinity concentration in units of mg/L as CaCO<sub>3</sub> (Section 2320 B).

Determine the dielectric constant E and then estimate A (see equations in Table 2330:1). Alternatively, use precalculated values of A in Table 2330:2 (e.g., A = 0.505 at 20 °C).

Next, estimate  $pf_m$  using the equation in Table 2330:1:

$$pf_m = 0.505 \times \left[ \frac{\sqrt{2.29 \times 10^{-2}}}{1 + \sqrt{2.29 \times 10^{-2}}} - 0.3(2.29 \times 10^{-2}) \right] = 0.063$$

Determine [HCO<sub>3</sub><sup>-</sup>] from Equation 4. Neglect  $Alk_o$ , but because the pH is >8.5, calculate the other terms. Table 2330:2 indicates that  $pK_2 = 10.38$  and  $pK_w = 14.16$ .

$$[HCO_3^{-}] = \frac{2.60 \times 10^{-3} + 10^{(0.063 - 9.00)} - 10^{(9.00 + 0.063 - 14.16)}}{1 + 2 \times 10^{[9.00 + 3(0.063) + 10.38]}}$$
$$= 2.30 \times 10^{-3} \text{ moles / L}$$

Therefore,  $p[HCO_3^-] = 2.64$ . Determine  $[Ca^{2+}]$  from Equation 3; neglect  $Ca_{in}$ :

$$[Ca^{2+}] = Ca_t = 3.80 \times 10^{-3} \text{ moles/L}$$

Therefore,  $p[Ca^{2+}] = 2.42$ .

Table 2330:2 indicates that the  $pK_s$  for calcite is 8.45. Determine  $pH_s$  using Equation 2:

$$pH_s = 10.38 - 8.45 + 2.42 + 2.64 + 5 (0.063) = 7.31$$

And finally, determine SI using Equation 1:

$$SI = 9.00 - 7.31 = 1.69$$

The positive SI indicates that the water is oversaturated with calcite.

2) Effects of neglecting  $Ca_{ip}$  and  $Alk_o$ —If  $Ca_{ip}$  is neglected, then  $pH_s$  is underestimated and SI is overestimated by  $p(1-Y_{Ca_{ip}})$ , where  $Y_{Ca_{ip}}$  is the fraction of total calcium in ion pairs. For example, if  $Y_{Ca_{ip}} = 0.30$  then the estimate for SI is 0.15 units too high. If  $Alk_o$  is neglected, then SI is overestimated by  $p(1-Y_{Alk_o})$ , where  $Y_{Alk_o}$  is the fraction of total alkalinity contributed by species other than  $HCO_3^-$ ,  $CO_3^{2-}$ ,  $OH_3^-$ , and  $H_3^+$ . The effects of neglecting  $Ca_{ip}$  and  $Alk_o$  are additive.

Nevertheless,  $Ca_{ip}$  and  $Alk_o$  may be neglected if  $Y_{Ca_{ip}}$  and  $Y_{Alk_o}$  are small and do not interfere with the interpretation of SI. These factors are usually small for natural waters with low TDS concentrations and neutral pH values, but may increase in some waters as pH values approach and exceed 9. At high pH values, however, SI is typically much larger than its overestimated index value, in which case neglecting  $Ca_{ip}$  and  $Alk_o$  is no problem. For instance, if the sample calculation in the example above was done using water-chemistry software (MINTEQA2) that considers  $Ca_{ip}$  and  $Alk_o$  (see Table 2330:3), SI would be 1.51 (0.18 units lower than the result obtained by hand calculations). In other words, neglecting  $Ca_{ip}$  and  $Alk_o$  did not interfere with interpreting the result; both calculations showed the water to be strongly oversaturated.

The potential for misinterpretation is most acute in nearly saturated waters with high sulfate concentration (e.g., recirculating cooling

Table 2330:2. Precalculated Values For pK and A at Selected Temperatures

Temperature			$pK_S$			
°C	$pK_2$	Calcite	Aragonite	Vaterite	$pK_w$	Α
0	10.63	8.38	8.22	7.74	14.94	0.489
5	10.55	8.39	8.24	7.77	14.73	0.493
10	10.49	8.41	8.26	7.80	14.53	0.496
15	10.43	8.43	8.28	7.84	14.34	0.501
20	10.38	8.45	8.31	7.87	14.17	0.505
25ª	10.33	8.48	8.34	7.91	13.99	0.510
30	10.29	8.51	8.37	7.96	13.83	0.514
35	10.25	8.54	8.41	8.00	13.68	0.520
40	10.22	8.58	8.45	8.05	13.53	0.525
45	10.20	8.62	8.49	8.10	13.39	0.531
50	10.17	8.66	8.54	8.16	13.26	0.537
60	10.14	8.76	8.64	8.28	13.02	0.549
70	10.13	8.87	8.75	8.40	_	0.563
80	10.13	8.99	8.88	8.55	_	0.578
90	10.14	9.12	9.02	8.70	_	0.593

Note: All values determined from the equations of Table 2330:1.

A is used to calculate  $pf_m$  (see Table 2330:1).

<sup>&</sup>quot;  $pf_m$  estimated from TDS values at 25 °C as follows:

TDS	$pf_m$
100	0.024
200	0.033
400	0.045
800	0.060
1000	0.066

water). The robust  $CaSO_4^0$  ion pair sequesters calcium, which can result in an SI overestimated by as much as 0.3 to 0.5 units, even at neutral pH. So SI may be thought to be zero (neither scale-forming nor corrosive) when in fact it is negative. To resolve this problem, determine  $pH_s$  using water-chemistry software that considers ion pairs and other forms of alkalinity (2330 D). Such calculations are most accurate when a complete mineral analysis is used.

Calcium complexed by organic matter and organic acid contributions to  $Alk_o$  can be difficult to characterize and integrate into water chemistry software. The fraction of calcium complexed by organic matter typically is expected to be small in distribution systems.<sup>4</sup> The contribution of organic acids to  $Alk_o$  can be significant in some waters<sup>5</sup> but will be small in natural waters with low concentrations of natural organic matter (NOM).

Another somewhat less rigorous procedure involves direct measurement of calcium ion activity  $\{Ca^{2+}\}$  with a calcium-specific ion electrode. Use Equation 6 to determine  $p[Ca^{2+}]$ ; then use  $p[Ca^{2+}]$  in Equation 2.

$$p\left[\operatorname{Ca}^{2+}\right] = p\left\{\operatorname{Ca}^{2+}\right\} - 4pf_m \tag{6}$$

This approach eliminates the need to determine  $Ca_{ip}$ .

 $Alk_o$  can be determined in organic-free waters if a complete mineral analysis is used with suitable chemical-equilibrium software. Alternatively,  $Alk_o$  can be determined either in organic-laden or organic-free waters as described below if carbonate alkalinity  $(Alk_c)$  can be obtained, where  $Alk_c$  is the alkalinity contributed by carbonate species  $(HCO_3^-)$  and  $CO_3^{2-}$ .  $Alk_c$  can

Table 2330:3. Graphical and Computer Methods That Can Be Used to Calculate CaCO<sub>3</sub> Saturation Indices

	CaCO <sub>3</sub> Indices  Basis for Calculation of SI CCPP						
Item <sup>a</sup>			Approximate Temperature Range °C	Approximate Limit of Ionic Strength	Ion Pairs Considered?	$\begin{array}{c} \operatorname{Alk}_o \\ \operatorname{Considered?} \end{array}$	Operating System
Caldwell-Lawrence Diagrams <sup>1-6</sup>	$pH_{sb}$	P, D	2–25	0.030	No	No	Graphical Diagrams
MINTEQA27,8	RS	P, D	0-100	0.5	Yes	Yes	Windows 98, NT, 2000, XP
PHREEQC <sup>9</sup>	RS	P, D	0–100	0.5	Yes	Yes	Windows 95, 98, NT 4.0, ME 2000, XP, Mac OS 9 and X, and Linux
PHREEQC Standard for high salinity waters <sup>9</sup>	RS	P, D	0–80	7–8	Yes	Yes	Windows 95, 98, NT 4.0, ME 2000, XP, Mac OS 9 and X, and Linux
WATEQ4F <sup>10</sup>	RS	D	0–100	0.5	Yes	Yes	Any PC capable of running DOS or MS DOS
MINEQL+11	RS	P, D	0-100	0.5	Yes	Yes	Windows 7, 8 and 10
Visual MINTEQ12	RS	P, D	0-100	0.5	Yes	Yes	Windows 7, 8 and 10

SI = saturation index; CCPP =  $CaCO_3$  precipitation potential;  $pH_{sb} = pH_s$  based on a hypothetical bicarbonate concentration calculated using the saturation pH; P = calculates amount of  $CaCO_3$  theoretically precipitated; P = calculates amount of P = calculates and P = calculates amount of P = calculates and P = calculates amount of P = calculates and P = calculates and P = calculates amount of P = calculates and P = cal

#### References

- 1. Loewenthal RE, Marais GVR. Carbonate chemistry of aquatic systems: theory and applications. Ann Arbor (MI): Ann Arbor Science Publishers, 1976. Note: Supplies 10.2- x 11.4-cm diagrams, with documentation.
- 2. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO3 films. Part 1: a practical approach for plant operators. 1977;69(11):592-599. Note: Provides 10.2-by 16.5-cm diagrams, with documentation.
- 3. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO3 films. Part II: a practical approach for plant operators. 1977;69(12):634-640. Note: Provides 10.2-by 16.5-cm diagrams, with documentation.
- 4. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO3 films. Part III: a practical approach for plant operators. 1978:70(1):12-18. Note: Provides 10.2- by 16.5-cm diagrams, with documentation.
- 5. Merrill DT. Conditioning for water softening and corrosion control. In: Sanks RL, ed. Water treatment plant design for the practicing engineer. Ann Arbor (MI): Ann Arbor Science Publishers, Inc.; 1978, p. 497.
- 6. Caldwell DH, Lawrence WB. Water softening and conditioning problems: solution by chemical equilibrium methods. Indust Engineer Chem. 45(3):535-548.
- 7. U.S. Environmental Protection Agency, Ecosystems Research Division, Center for Exposure Assessment Modeling (CEAM). http://www2.epa.gov/exposure-assessment-models/minteqa2 [Accessed February 2021]. Note: Links to software and documentation.
- 8. Allison JD, Brown DS, Novo-Gradac KJ. MINTEQA2/PRODEFA2: a geochemical assessment model for environmental systems: version 3.0 user's manual; EPA/600/3-91/021. Athens (GA): U.S. Environmental Protection Agency, Environmental Research Laboratory, Office of Research and Development; 1991.
- 9. U.S. Geological Survey, Branch of Information Services. http://wwwbrr.cr.usgs.gov/projects/GWC\_coupled/phreeqc/index.html [accessed February 2021]. Note: Links to software and documentation
- 10. U.S. Geological Survey. http://wwwbrr.cr.usgs.gov/projects/GWC\_chemtherm/software.htm [accessed January 2017].
- Schecher WD, McAvoy DC. MINEQL: a chemical equilibrium modeling system: version 5.0 for Windows user's manual. 3<sup>rd</sup> ed. Hallowell (ME): Environmental Research Software; 2015. Environmental Research Software. http://www.mineql.com/. Accessed March 2021. Note: Provides links to purchase software and documentation.
- 12. John Peter Gustafsson at KTH Royal Institute of Technology. http://vminteq.lwr.kth.se/ [accessed February 2021]. Note: Links to software and documentation.

be calculated if the total inorganic carbon ( $C_t$ ) concentration is known, where  $C_t$  is the sum of the carbonate species [CO<sub>2(aq)</sub>, H<sub>2</sub>CO<sub>3</sub>, HCO<sub>3</sub><sup>-</sup>, and CO<sub>3</sub><sup>2-</sup>].  $C_t$  is also known as *dissolved inorganic carbon* (DIC). Some total organic carbon (TOC) analyzers can measure  $C_t$  via acidification, purging, and CO<sub>2(g)</sub> detection.

 $\mathrm{CO}_{2(g)}$  detection with nondispersive infrared (NDIR) sensors virtually eliminates interference from other volatile compounds at low pH (e.g., purgeable organic carbon, hydrogen sulfide) because the sensors use wavelengths that select for  $\mathrm{CO}_{2(g)}$  absorbance. Conductivity-based  $\mathrm{CO}_{2(g)}$  detection with a gas-permeable membrane will register interference from volatile weak acids (e.g., hydrogen sulfide), but this interference is negligible for typical waters. If  $C_t$  is obtained, calculate  $Alk_c$  as follows:

$$Alk_c = C_t \left( \frac{10^{(pf_m - pH - pK_1)} + 2 \times 10^{(4pf_m - pK_1 - pK_2)}}{10^{-2pH} + 10^{(pf_m - pH - pK_1)} + 10^{(4pf_m - pK_1 - pK_2)}} \right)$$

where:

 $K_1$  = first dissociation constant for carbonic acid, including  ${
m CO}_{2(aq)}$ , at water temperature.

Estimate  $Alk_o$  by subtracting  $Alk_c$  from  $Alk_t$  (i.e.,  $Alk_o = Alk_t - Alk_o$ ).

Alternatively, bypass the determination of  $Alk_o$  and substitute  $Alk_c$  for the quantity " $Alk_t - Alk_o$ " in Equation 4 when estimating [HCO<sub>3</sub>].

b. Graphical solutions for saturation pH: Caldwell–Lawrence diagrams can be used to determine a saturation pH<sup>7-11</sup>; however, graphical methods do not follow the definition of  $pH_s$  provided in Equation 2. In graphical methods, the bicarbonate term is a hypothetical quantity calculated as a function of saturation pH; in Equation 2, the calculated bicarbonate concentration is a function of measured pH (see 2330 D). The diagrams can be particularly useful for estimating the chemical dosages needed to achieve desired water conditions. See 2330 D for more information about

Table 2330:4. Quality Assurance/Quality Control Examples for Saturation Index by Calculation

Parameter (units)			Values		
Example	Aª	В	С	D	Е
			Input		
Calcium (mg/L)	152	10	90	90	152
Magnesium (mg/L)	39	2	_	_	39
Sodium (mg/L)	50	10	_	_	50
Potassium (mg/L)	5	1		_	5
Chloride (mg/L)	53	5	-	-	53
Alkalinity (mg/L as CaCO <sub>3</sub> )	130	30	200	200	130
Sulfate (mg/L)	430	10	_	_	430
Silica (mg/L as SiO <sub>2</sub> )	15	0	_	_	15
рН	9.00	9.20	7.20	7.20	9.00
Temperature (°C)	20	15	25	25	20
Alk <sub>0</sub> (mg/L as CaCO <sub>3</sub> )	Neglected	Neglected	Neglected	Neglected	6
Ca <sub>ip</sub> (mg/L as Ca)	Neglected	Neglected	Neglected	Neglected	49
TDS (mg/L)	_	-	750	-	-
EC (µS/cm)	_	· —	_	1230	_
			Output		
I (M) <sup>b</sup>	$2.30 \times 10^{-2}$	$1.47 \times 10^{-3}$	$1.88 \times 10^{-2}$	$3.08 \times 10^{-2}$	$2.30 \times 10^{-2}$
[HCO <sub>3</sub> <sup>-</sup> ] (M)	$2.29 \times 10^{-3}$	$5.22 \times 10^{-4}$	$3.99 \times 10^{-3}$	$3.99 \times 10^{-3}$	$2.19 \times 10^{-3}$
$[Ca^{2+}](M)$	$3.79 \times 10^{-3}$	$2.50 \times 10^{-4}$	$2.25 \times 10^{-3}$	$2.25 \times 10^{-3}$	$2.57 \times 10^{-3}$
$pH_{\mathcal{S}}$	7.30	8.79	7.19	7.25	7.49
SI	1.70	0.23	0.01	0.05	1.51

<sup>&</sup>lt;sup>a</sup> The result differs from the example presented earlier due to rounding in the hand calculations.

the diagrams; consult the references for descriptions of how to use them.

# 3. Saturation Index by Experimental Determination

a. Saturometry: Saturometers were developed to measure the degree of CaCO<sub>3</sub> saturation in seawater. Analysts equilibrate CaCO<sub>3</sub> with a water of known calcium concentration and pH in a sealed flask containing a pH electrode. The water temperature is controlled by a constant-temperature bath. During equilibration, pH decreases if CaCO<sub>3</sub> precipitates and increases if it dissolves. Equilibrium is said to have been achieved when the pH stops changing. The initial pH and calcium concentration values and the final pH value are used to estimate the carbonate concentration, which can be used to estimate RS.<sup>12</sup> Equation 7 (2330 D.1) may then be used to determine SI.

A major advantage of this method is that the approach to equilibrium can be tracked by measuring pH, thus minimizing uncertainty about achieving equilibrium. The method is most sensitive in the range of minimum buffering intensity (pH 7.5 to 8.5). Although the calculations do not consider ion pairs or  $Alk_o$ , these can be included so long as their pH dependence is known. The technique has been used for *in situ* oceanographic measurements, <sup>13</sup> as well as in the laboratory.

The saturometry calculations discussed above use the  $K_s$  of the CaCO<sub>3</sub> phase assumed to control solubility. Uncertainties occur if the controlling solid is unknown. To resolve such uncertainties, measure  $K_s$  of the controlling solid; it is equal to the CaCO<sub>3</sub> activity product (Ca<sup>2+</sup> × CO<sub>3</sub><sup>2-</sup>) at equilibrium. Calculate the latter from the equilibrium pH and initial calcium concentration, alkalinity, and pH measurements.<sup>14</sup>

b. Alkalinity difference technique: <sup>15</sup> SI also can be determined by equilibrating water of known pH, calcium concentration, and alkalinity with  $CaCO_3$  in a sealed, constant-temperature system. The  $CaCO_3$  activity product before equilibration is determined from initial calcium, pH, and alkalinity (or total carbonate) values. The  $CaCO_3$  solubility product constant ( $K_s$ ) equals the  $CaCO_3$  activity product after equilibration, which is determined by using the alkalinity change that occurred during equilibration. RS is found by dividing the initial activity product by  $K_s$ . Calculate SI using Equation 7 (2330 D.1). The advantage of this method is that it makes no assumptions about the identity of the  $CaCO_3$  phase. However, it is more difficult to determine when equilibrium is achieved with this method than with the saturometry method.

Whatever the method used, use temperatures that are the same as that of the water of interest. Alternatively, correct test results to the temperature of the water of interest.<sup>15</sup>

## 4. Quality Assurance/Quality Control

If the calculations in the "Saturation Index by Calculation" section are automated (e.g., in a spreadsheet), check that the equations were properly programmed with the data in Table 2330:4.

- Ryznar JW. A new index for determining the amount of calcium carbonate formed by a water. J Amer Water Works Assoc. 1944;36(4):472–483.
- Snoeyink VL, Jenkins D. Water chemistry. New York (NY): John Wiley & Sons; 1980.

<sup>&</sup>lt;sup>b</sup> Assuming all the alkalinity is due to bicarbonate ion, a charge of 2 for Ca<sub>ip</sub>, and a charge of 1 for Alk<sub>o</sub>.

- Kenny JD, Hokanson DR, Trussell RR. Technical note: calculation of the Langelier index at high pH. J Amer Water Works Assoc. 2015;107(3):82–S3.
- Snoeyink VL, Wagner I. Principles of corrosion of water distribution systems. In: Internal corrosion of water distribution systems, 2nd ed. Report No. 90508. Denver (CO): American Water Works Association; 1996.
- 5. Hunt CW, Salisbury JE, Vandemark D. Contribution of non-carbonate anions to total alkalinity and overestimation of  $pCO_2$  in New England and New Brunswick rivers. Biogeosciences. 2011; 8:3069–3076.
- Garrels RM, Christ CL. Solutions, minerals, and equilibria. New York (NY): Harper & Row; 1965.
- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. I. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(11):592–599.
- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. II. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(12):634–640.

- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. III. A practical approach for plant operators. J Amer Water Works Assoc. 1978;70(1):12–18.
- Loewenthal RE, Marais GVR. Carbonate chemistry of aquatic systems: theory and applications. Ann Arbor (MI): Ann Arbor Science Publishers, 1976.
- Merrill DT. Chemical conditioning for water softening and corrosion control. In: Sanks RL, ed. Water treatment plant design. Ann Arbor (MI): Ann Arbor Science Publishers; 1976.
- Ben-Yaakov S, Kaplan IR. Determination of carbonate saturation of seawater with a carbonate saturometer. Limnol Oceanogr. 1969:14(6):874–882.
- Ben-Yaakov S, Kaplan IR. Deep-sea in situ calcium carbonate saturometry. J Geophys Res. 1971;76(3):722–731.
- Plath DC, Johnson KS, Pytkowicz RM. The solubility of calcite probably containing magnesium—in seawater. Marine Chem. 1980;10(1):9–29.
- Balzar W. Calcium carbonate saturometry by alkalinity difference. Oceanol Acta. 1980;3:237.

# (2330) C. Indices Predicting the Quantity of $CaCO_3$ That Can Be Precipitated or Dissolved

The calcium carbonate precipitation potential (CCPP) predicts both the water's tendency to precipitate or dissolve CaCO<sub>3</sub> and the amount that may be precipitated or dissolved. The CCPP also is called calcium carbonate precipitation capacity (CCPC).

CCPP is the quantity of CaCO<sub>3</sub> that theoretically can be precipitated from oversaturated waters or dissolved by undersaturated waters during equilibration. <sup>1-3</sup> The amount that actually precipitates or dissolves may be more or less for several possible reasons, including

- · equilibrium may not be achieved;
- · temperature and ionic strength approximations;
- failure to accurately account for complexation of species involved in the reaction;
- · the presence of threshold inhibitors;
- inaccurate assumptions about the solid phase that forms;
- inaccurate solubility constants, dissociation constants, or measurements; and
- differences in concentrations between the bulk phase and local environments.<sup>4</sup>

CCPP is negative for undersaturated waters, zero for saturated waters, and positive for oversaturated waters.

#### 1. Calculating CCPP

The CCPP does not lend itself to hand calculations. Preferably calculate CCPP using computerized water chemistry models, spreadsheets, 5.6. or Caldwell–Lawrence diagrams (see 2330 D). The most reliable calculations consider ion pairs and the alkalinity contributions of other species besides HCO<sub>3</sub><sup>-</sup>, CO<sub>3</sub><sup>2-</sup>, OH<sup>-</sup>, and H<sup>+</sup>. Models that do not consider these factors overestimate how much CaCO<sub>3</sub> can be precipitated and underestimate how much can be dissolved.

## 2. Experimental Determination of CCPP

Estimate CCPP by one of several experimental techniques.

- a. Saturometry: See 2330 B.3a. The CCPP is determined as part of the RS calculation.
- b. Alkalinity-difference technique: See 2330 B.3b. The CCPP equals the difference between the initial and equilibrated water's alkalinity (or calcium) values, when expressed as CaCO<sub>3</sub>.
- c. Marble test: The marble test<sup>1-3,7-10</sup> is similar to the alkalinity-difference technique. The CCPP equals the change in alkalinity (or calcium) values during equilibration, when expressed as CaCO<sub>3</sub>.
- d. Enslow test: The Enslow test<sup>10</sup> is a continuous version of the alkalinity-difference or marble tests. Water is fed continuously to a leveling bulb or separatory funnel partly filled with CaCO<sub>3</sub>. Bulb or funnel effluent is then is filtered through the crushed marble so that the filtrate is assumed to be in equilibrium with CaCO<sub>3</sub>. The CCPP equals the change in alkalinity (or calcium) that occurs when water passes through the apparatus.
- e. Calcium carbonate deposition test. The calcium carbonate deposition test (CCDT) is an electrochemical method that measures the electric current produced when DO is reduced on a rotating electrode. When an oversaturated water is placed in the apparatus, it deposits CaCO<sub>3</sub> on the electrode, interfering with oxygen transfer and diminishing the current. The CaCO<sub>3</sub> deposition rate is directly proportional to the rate at which current declines. The CCDT and the CCPP are related but not identical: CCDT is a rate and CCPP is a quantity.

For realistic assessments of the CCPP (or CCDT), keep the test temperature the same as the water-source temperature or else correct the test results to water-source temperature.

- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. I. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(11):592–599.
- Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. II. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(12):634–640.

- 3. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. III. A practical approach for plant operators. J Amer Water Works Assoc. 1978;70(1):12-18.
- 4. Randtke SJ. Precipitation, co-precipitation, and precipitative softening. In: Edzwald JK, ed. Water quality & treatment; a handbook on drinking water, 6th ed. New York (NY): McGraw Hill; 2011, p. 13.26.
- 5. Trussell RR. Spreadsheet water conditioning, J Amer Water Works Assoc. 1998;90(6):70.
- 6. Holm TR, Schock MR. 1998. Computing SI and CCPP using spreadsheet programs. J Amer Water Works Assoc. 90(7):80-89.

- 7. Merrill DT. Chemical conditioning for water softening and corrosion control. In: Sanks RL, ed. Water treatment plant design. Ann Arbor (MI): Ann Arbor Science Publishers; 1976.
- 8. De Martini F. Corrosion and the Langelier calcium carbonate saturation index. J Amer Water Works Assoc. 1938;30(1):85-111.
- 9. Hoover CP, Langelier WF. Practical application of the Langelier method. J Amer Water Works Assoc. 1938;30:1802-1807.
- 10. Dye JF, Tuepker JL. Chemistry of the lime-soda process. In: American Water Works Association, Water quality and treatment: a handbook of public water supplies, 3rd ed. New York (NY): McGraw-Hill Book Co.: 1971.
- 11. McClelland NI, Mancy KH. CCDT bests Ryznar index as pipe CaCO<sub>3</sub> film predictor. Water Sewage Works. 1979;126:77.

# 2330) D. Graphical and Computer Methods for CaCO3 Indices

# 1. Description

Table 2330:3 lists some of the graphical and computer methods that can be used to determine SI and CCPP. It also provides a brief description of their characteristics.

Many computer methods calculate RS instead of calculating SI directly. When RS data are presented, calculate SI from:1

$$SI = log_{10}RS \tag{7}$$

where:

RS = ratio of CaCO<sub>3</sub> activity product to CaCO<sub>3</sub> solubility product constant.

The graphical methods use a hypothetical bicarbonate concentration calculated at the saturation pH (i.e., they implicitly define saturation pH as the pH the water would exhibit if it were in equilibrium with  $CaCO_3$  at existing calcium, total alkalinity, and  $C_t$ concentrations), while the bicarbonate concentration in Equation 2 is calculated at the measured value of pH.<sup>1,2</sup> Basing the saturation index on a hypothetical bicarbonate concentration calculated at the saturation pH not only yields different values but also causes the sign of the index to reverse when the pH is greater than the CaCO<sub>3</sub> system's second saturation point, which can occur at a pH of approximately  $pK_2$ . When sign reversal occurs, a positive value of SI (not the usual negative value) connotes an undersaturated water.3 When SI, pH<sub>s</sub>, or RS is calculated according to the equations in 2330 B, sign reversal does not occur, thereby eliminating the confusing sign change. Furthermore, the SI and RS values thereby obtained are directly related to the Gibbs free energy (driving force) of the reaction<sup>4-6</sup> and fundamentally consistent with the saturation indices used in numerous other applications.<sup>7</sup>

Some computer methods not listed in Table 2330:3 use Equation 5 (the simplified version of Equation 2), in which bicarbonate is assumed to equal alkalinity. As discussed in 2330 B.2a, when pH is approximately neutral (6.0 to 8.5) and alkalinity is more than about 50 mg/L as CaCO3, Equations 2 and 5 yield virtually equal values of  $pH_s$  because total alkalinity is due almost entirely to the bicarbonate ion. When pH is more than about 8.5, avoid using Equation 5 and only use Equation 7 with SI values determined using Equation 2.

Using a graphical or computer method that calculates  $pH_s$ from Equation 2, or RS, is strongly recommended. Table 2330:3 identifies the saturation pH basis used for each graphical and computer method listed.

Some models only calculate the amount of CaCO<sub>3</sub> that can be precipitated, not the amount that can be dissolved. Others calculate both.

Graphical and computer methods can be used to determine many more parameters than CaCO3 saturation indices. A fee may be charged for computer software or graphs. Table 2330:3 describes parameters each code uses to calculate SI. Refer to the sources in the table footnotes for current information.

- 1. Snoeyink VL, Jenkins D. Water chemistry. New York (NY): John Wiley & Sons; 1980.
- 2. Rossum JR, Merrill DT. An evaluation of the calcium carbonate saturation indexes. J Amer Water Works Assoc. 1983;75(2):95-100.
- 3. Loewenthal RE, Marais GVR. Carbonate chemistry of aquatic systems: theory and applications. Ann Arbor (MI): Ann Arbor Science Publishers, 1976.
- 4. Trussell RR, Russell LL, Thomas JF. The Langelier Index. In: Proceedings of the AWWA Water Quality Technology Conference; Kansas City (MO); 1977 Dec 4-7. Denver (CO): American Water Works Association; 1977.
- 5. Crittenden JC, Trussell RR, Hand DH, Howe KJ, Tchobanoglous G. MWH's Water treatment: principles and design, 3rd ed. Hoboken (NJ): John Wiley & Sons, Inc.; 2012.
- 6. Randtke SJ. Precipitation, co-precipitation, and precipitative softening. In: Edzwald JK, ed. Water quality & treatment: a handbook on drinking water, 6th ed. New York (NY): McGraw Hill; 2011, p.
- 7. DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. I. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(11):592-599.
- 8. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. II. A practical approach for plant operators. J Amer Water Works Assoc. 1977;69(12):634-640.
- 9. Merrill DT, Sanks RL. Corrosion control by deposition of CaCO<sub>3</sub> films. III. A practical approach for plant operators. J Amer Water Works Assoc. 1978;70(1):12–18.
- 10. Merrill DT. Chemical conditioning for water softening and corrosion control. In: Sanks RL, ed. Water treatment plant design. Ann Arbor (MI): Ann Arbor Science Publishers, 1976.
- 11. Caldwell DH, Lawrence WB. Water softening and conditioning problems: solution by chemical equilibrium methods. Indust Eng Chem. 1953;45(3):535-548.